

# Aqueous Dispersions of Polypropylene and Poly(1-butene) with Variable Microstructures Formed with Neutral Nickel(II) Complexes

Peter Wehrmann and Stefan Mecking\*

Universität Konstanz, Fachbereich Chemie,  
Universitätsstrasse 10, D-78457 Konstanz, Germany

Received June 29, 2006

Revised Manuscript Received July 17, 2006

Polymerization of 1-olefins and the polymer microstructures formed have been studied intensively with early transition metal catalysts, and more recently with late transition metal cationic Ni(II) and Pd(II) diimine complexes.<sup>1,2</sup> In contrast, while neutral Ni(II) polymerization catalysts are of general interest due to their specific functional group tolerance, they have been little studied for 1-olefin polymerization.<sup>3–5</sup> The only notable study is Fink's polymerization of C<sub>4</sub> to C<sub>20</sub> 1-olefins (in a nonaqueous system) with an in situ catalyst [Ni<sup>0</sup>(cod)<sub>2</sub>]/(Me<sub>3</sub>Si)<sub>2</sub>N-P[=NSiMe<sub>3</sub>)<sub>2</sub> that most likely contains neutral Ni(II) active sites. 2,ω-incorporation was observed exclusively.<sup>3–5</sup>

Polymer dispersions, that is aqueous dispersions of polymer particles with sizes of ca. 50 nm to 1 μm, are employed on a large scale e.g. for environmentally friendly coatings and paints.<sup>6</sup> Catalytic synthesis of polymer dispersions is an attractive aim, as it can enable control of polymer microstructures, by contrast to currently practiced free radical emulsion polymerization.<sup>7–11</sup> Moreover, 1-olefins in particular are not susceptible to radical polymerization due to stable radical formation.

Complexes [{κ<sup>2</sup>-N,O-6-C(H)=NAr-2,4-R'<sub>2</sub>C<sub>6</sub>H<sub>3</sub>O}NiMe(L)] (Ar = 2,6-{3,5-R<sub>2</sub>C<sub>6</sub>H<sub>3</sub>)<sub>2</sub>C<sub>6</sub>H<sub>3</sub>; **1**: L = tmeda, R = CH<sub>3</sub>, R' = I; **2**: L = tmeda, R = CF<sub>3</sub>, R' = 3,5-(F<sub>3</sub>C)<sub>2</sub>C<sub>6</sub>H<sub>3</sub>; **3**: L = tmeda, R = CF<sub>3</sub>, R' = I; tmeda = N,N,N',N'-tetramethylethylenediamine) in ethylene polymerization afford a range of microstructures depending on the remote substituents R (**1**, highly branched polymer; **3**, nearly linear).<sup>12</sup> **1** has a high capability for chain running, and for insertion of ethylene into secondary metal alkyls, which prompted us to study 1-olefin polymerization.

Exposure of **1–3** to 1-butene indeed resulted in the formation of low-molecular-weight polymers (Table 1). Productivities up to 10<sup>3</sup> TO (TO = turnover = mole monomer converted per mole of Ni) are observed, vs 10<sup>5</sup> TO in ethylene polymerization. The question arises whether catalyst deactivation occurs (intrinsically or, e.g., by impurities in the monomer) or whether chain growth is slow. Monitoring a reaction by continuously drawing samples reveals that polymerization continues for hours (Figure 1). By comparison to ethylene polymerization, insertion of the bulky 1-olefin into a Ni(II) alkyl bond slows down chain growth. Accordingly, **1** which has a pronounced capability for chain running (vide supra) to form a less hindered species after 1-olefin insertion is the most active. Molecular weight is time-independent, that is chain transfer controls molecular weights. In accordance with this, the calculated number of chains formed per nickel(II) center present in the reaction mixture is ≫ 1, on the order of 10<sup>2</sup>.

To prepare polymer dispersions, a high degree of dispersion of the catalyst in the initial reaction mixture is a prerequisite.<sup>7,8,11</sup> To a mixture of an aqueous surfactant solution and a solution

Table 1. Polymerization Results<sup>a</sup>

no.	mon.	cat. (μmol)	yield [g]	TON <sup>d</sup>	M <sub>n</sub> (M <sub>w</sub> /M <sub>n</sub> ) <sup>e</sup> [10 <sup>3</sup> g mol <sup>-1</sup> ]	1,2 <sup>f</sup>	2,ω <sup>f</sup>	1,ω <sup>f</sup>
1 <sup>b</sup>	B	<b>1</b> (40)	1.5	670	0.5 (3.3)	n.d.	n.d.	n.d.
2 <sup>b</sup>	B	<b>1</b> (42)	3.2	1360	1.0 (3.5)	10%	65%	25%
3 <sup>b</sup>	B	<b>2</b> (60)	1.5	450	1.4 (1.9)	50%	22%	28%
4 <sup>b</sup>	B	<b>3</b> (80)	1.5	340	1.2 (1.9)	73%	13%	14%
5 <sup>b</sup>	P	<b>3</b> (80)	1.5	450	0.6 (1.3)	90%		10%
6 <sup>b</sup>	H	<b>1</b> (40)	0.3	90	0.5 (1.7)	27%	41%	32%
7 <sup>c</sup>	B	<b>1</b> (80)	3.2	710	1.6 (1.9)	11%	66%	23%
8 <sup>c</sup>	B	<b>3</b> (94)	0.7	130	1.1 (1.6)	65%	13%	21%
9 <sup>c</sup>	P	<b>3</b> (94)	0.4	100	0.4 (1.7)	79%		21%

<sup>a</sup> 5 °C (entry 1: 20 °C); reaction time: 16 h (entry 1), 64 h (entries 2 and 3), 120 h (entries 4 and 8), 200 h (entry 5), 83 h (entry 6), 41 h (entries 7), 167 h (entry 9). <sup>b</sup> 10 mL of toluene; monomer = 30 g (entry 1), 50 g (entries 2–4), 40 g (entry 5), 65 g (entry 6). <sup>c</sup> 120 mL of water; 0.9 g of SDS; 2 mL of toluene; 0.1 mL of hexadecane (entry 9: 200 mL water; 1.5 g of SDS); monomer = 7.7 g (entry 7), 6.3 g (entry 8), 8.0 g (entry 9). <sup>d</sup> mol [1-olefin] × mol<sup>-1</sup> [Ni]. <sup>e</sup> From GPC vs linear PE standards at 160 °C. <sup>f</sup> Incorporation mode.

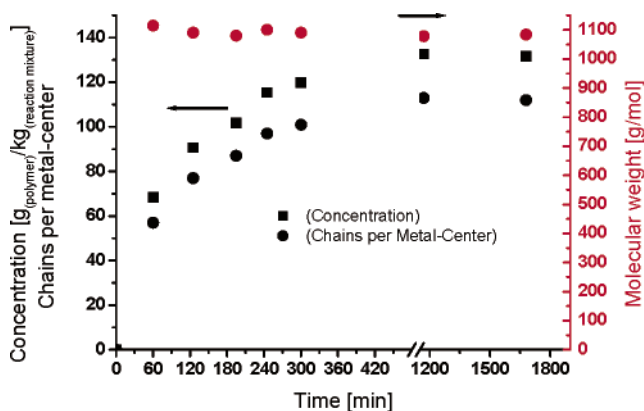
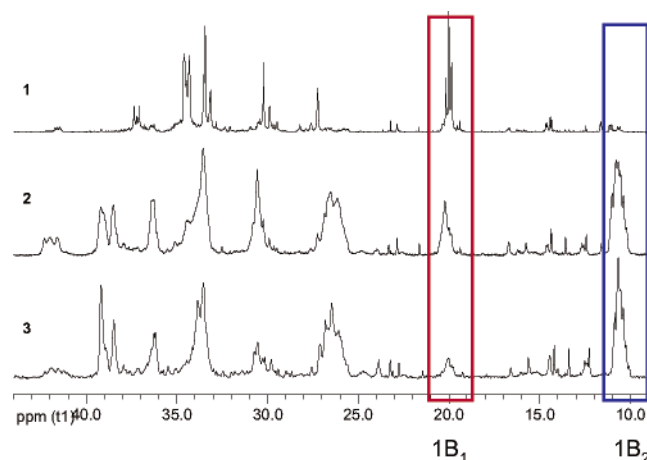


Figure 1. Polymer formation over time; time-dependent molecular weights and calculated number of polymer chains per Ni center present in the reaction mixture (99 μmol of **1**, 80 g of 1-butene, and 9 g of toluene, at 5 °C).

of **1**, **2**, or **3** in a small amount of toluene a metered amount of liquid monomer was added (vapor pressure of 1-butene at 20 °C, 2 bar; vapor pressure of propylene, 9 bar). The mixture was sheared intensively by an ultrasound device in the pressure reactor, to form a miniemulsion. Colloidally stable dispersions were obtained (entries 7–9). Polymer solids content of entry 7 was 2.6 wt %. Volume average particles sizes, as determined by dynamic light scattering, are 50–100 nm. Catalyst activity is somewhat lowered by comparison to nonaqueous polymerizations. This is likely due to a partial, reversible or irreversible, deactivation of the catalyst by water<sup>13</sup> (note that reaction conditions in terms of monomer concentration in the organic phase are similar in aqueous and nonaqueous polymerizations). However, half-lives for deactivation in the aqueous system must be on the order of at least an hour.<sup>14</sup>

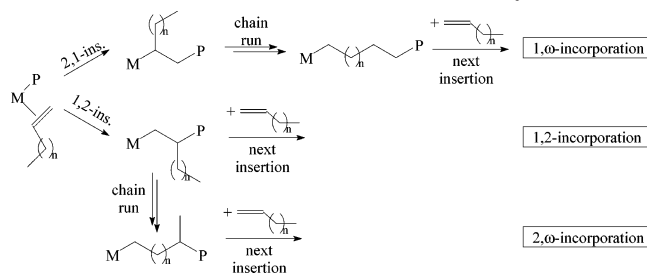
Microstructures of the poly(1-olefins) were studied by <sup>13</sup>C NMR spectroscopy. Unexpectedly in view of Fink's findings, 1,2-, 2,ω-,<sup>15</sup> and also 1,ω-incorporation are found (Table 1 and Figure 2; cf. Supporting Information for NMR details). Concerning the underlying insertion steps, 1,2-insertion is well documented for catalytic polymerization, and observation of 2,ω-incorporation shows it to occur also with these neutral Ni(II) complexes. 1,ω incorporation shows that 2,1-insertion of olefin also occurs to a significant extent. The absence of ethyl and propyl branches in poly(1-hexene) shows that after a 1,2-

\* Corresponding author. E-mail: stefan.mecking@uni-konstanz.de.



**Figure 2.**  $^{13}\text{C}$  NMR spectra of poly(1-butene)s prepared with different catalyst precursors (1B<sub>1</sub>,  $-\text{CH}_3$  of a methyl branch; 1B<sub>2</sub>,  $-\text{CH}_3$  of an ethyl branch). For full assignments see the Supporting Information).

**Scheme 1. Mechanism of Chain Growth ( $P$  = Polymer Chain)**



insertion either the next insertion occurs (1,2-incorporation; Scheme 1), or chain running will go all the way to the end of the branch to form a primary alkyl prior to the next insertion (2, $\omega$ -incorporation). The latter makes it seem likely that 2,1-insertion will also be followed by chain running to form a primary metal-alkyl, that is result in 1, $\omega$ -incorporation exclusively. Overall, insertion occurs only in primary metal alkyls.  $^1\text{H}$  NMR spectra of polypropylene show vinyl end groups  $-\text{CH}_2\text{CH}=\text{CH}_2$ , trisubstituted  $-\text{CH}=\text{CMe}_2$ , internal olefin  $-\text{CH}=\text{CH}-$  and vinylidene groups  $-\text{CH}_2\text{C}(\text{Me})=\text{CH}_2$  (the latter two predominating), confirming both 1,2- and 2,1-insertion to occur. Poly(1-butene) possesses analogous end groups (Supporting Information). That 2,1-insertion does not occur in Fink's system can be due to the high steric crowding of the Ni center by the  $\kappa^2\text{-}N,N$  ligand.<sup>5b</sup>

Remarkably, the microstructures are dependent on the catalyst (Table 1 and Figure 2). Whereas 1,2-incorporation prevails in poly(1-butene) prepared with **3** (73%), **1** affords 2, $\omega$ -incorporation preferentially (65%). As outlined, 1,2-insertion prevails with all catalysts, and the preference for 2, $\omega$ -incorporation of **1** is due to a high propensity to run even past a tertiary carbon. The high capability of **1** to chain run to a less hindered  $\text{M}-\text{CH}_2-\text{CH}_2\text{R}$  is also in accord with the higher activity observed in 1-butene polymerization (Table 1).<sup>16</sup> It also agrees with the high chain running capability of **1** observed in ethylene polymerization.<sup>12</sup>

In summary, 1-olefins are polymerized by the neutral Ni(II) complexes studied. Polymerizations in aqueous emulsions, starting from a monomer miniemulsion, afford dispersions of poly(1-olefins). Microstructure analyses reveal that insertion occurs in primary alkyls exclusively, formed by 1,2- and 2,1-insertion, and subsequent chain running. 2,1-insertion has been unambiguously shown for a neutral Ni(II) polymerization catalyst for the first time. Microstructures can be varied by

control of the chain running capability of the catalyst via remote substituents of the salicylaldimine ligand.

**Acknowledgment.** Financial support by BASF AG is gratefully acknowledged. We thank Lars Bolk for GPC analyses. S.M. is indebted to the Fonds der Chemischen Industrie and to the Hermann Schnell Foundation.

**Supporting Information Available:** Text giving general methods and materials and figures showing NMR spectra of polymers and assignments and DSC plots. This material is available free of charge via the Internet at <http://pubs.acs.org>.

**References and Notes**

- (1) *Ziegler Catalysts*; Fink, G., Mülhaupt, R., Brintzinger, H. H., Eds.; Springer: Berlin, 1995.
- (2) (a) Killian, C. M.; Tempel, D. J.; Johnson, L. K.; Brookhart, M. *J. Am. Chem. Soc.* **1996**, *118*, 11664–11665. (b) McCord, E. F.; McLain, S. J.; Nelson, L. T. J.; Arthur, S. D.; Coughlin, E. B.; Ittel, S. D.; Johnson, L. K.; Tempel, D. J.; Killian, C. M.; Brookhart, M. *Macromolecules* **2001**, *34*, 362–371. (c) Pellecchia, C.; Zambelli, A. *Macromol. Rapid Commun.* **1996**, *17*, 333–338. (d) Cherian, A. E.; Rose, J. M.; Lobovsky, E. B.; Coates, G. W. *J. Am. Chem. Soc.* **2005**, *127*, 13770–13771. Also cf. polymerization of 2-butene: (e) Leatherman, M. D.; Brookhart, M. *Macromolecules* **2001**, *34*, 2748–2750. (f) Cherian, A. E.; Lobovsky, E. B.; Coates, G. W. *Chem. Commun.* **2003**, 2556–2557. Review: (g) Ittel, S. D.; Johnson, L. K.; Brookhart, M. *Chem. Rev.* **2000**, *100*, 1169–1203.
- (3) (a) Younkin, T. R.; Connor, E. F.; Henderson, J. I.; Friedrich, S. K.; Grubbs, R. H.; Bansleben, D. A. *Science* **2000**, *287*, 460–462. (b) Connor, E. F.; Younkin, T. R.; Henderson, J. I.; Hwang, S. J.; Roberts, W. P.; Litzau, J. J.; Grubbs, R. H. *J. Polym. Sci., Part A*, **2002**, *40*, 2842–2854.
- (4) Note that lacking incorporation of the 1-olefin product is the basis for the SHOP process for ethylene oligomerization: *Multiphase Homogeneous Catalysis*; Cornils, B.; Herrmann, W. A.; Horvath, I. T.; Leitner, W.; Mecking, S.; Olivier-Bourbigou, H.; Vogt, D., Eds.; VCH: Weinheim, **2005**, pp 330–334.
- (5) (a) Moehring, V. M.; Fink, G. *Angew. Chem.* **1985**, *97*, 982–984; *Angew. Chem., Int. Ed. Engl.* **1985**, *24*, 1001–1003. (b) Schubbe, R.; Angermund, K.; Fink, G.; Goddard, R. *Macromol. Chem. Phys.* **1995**, *196*, 467–478.
- (6) (a) *Emulsion Polymerization and Emulsion Polymers*; Lovell, P. A., El-Aasser, M. S., Eds.; Wiley: Chichester, U.K., 1997. (b) *Wässrige Polymerdispersionen*; Distler, D., Ed.; VCH: Weinheim, Germany, 1999.
- (7) (a) Bauers, F. M.; Mecking, S. *Macromolecules* **2001**, *34*, 1165–71. (b) Bauers, F. M.; Mecking, S. *Angew. Chem., Int. Ed.* **2001**, *40*, 3020–3022. (c) Monteil, V.; Wehrmann, P.; Mecking, S. *J. Am. Chem. Soc.* **2005**, *127*, 14568–14569. (d) Göttker-Schnetmann, I.; Korthals, B.; Mecking, S. *J. Am. Chem. Soc.* **2006**, *128*, 7708–7709. (e) Mecking, S.; Monteil, V.; Huber, J.; Kolb, L.; Wehrmann, P. *Makromol. Symp.* **2006**, *236*, 117–123.
- (8) (a) Soula, R.; Novat, C.; Tomov, A.; Spitz, R.; Claverie, J.; Drujon, X.; Malinge, J.; Saudemont, T. *Macromolecules* **2001**, *34*, 2022–2026. (b) Soula, R.; Sailard, B.; Spitz, R.; Claverie, J. *Macromolecules* **2002**, *35*, 1513–1523.
- (9) (a) Ono, H.; Kato, T. *J. Polym. Sci., Part A: Polym. Chem.* **2000**, *38*, 1083–1089. (b) Monteil, V.; Bastero, A.; Mecking, S. *Macromolecules* **2005**, *38*, 5393–5399.
- (10) (a) Lu, S.-Y.; Quayle, P.; Booth, C.; Yeates, S. G.; Padget, J. C. *Polym. Int.* **1993**, *32*, 1–4. (b) Kühn, I.; Mohr, B.; Durant, Y.; Schwab, R.; Leyrer, R. (BASF) DE 19859191, 2000. (c) Claverie, J. P.; Viala, S.; Maurel, V.; Novat, C. *Macromolecules* **2001**, *34*, 382–388. (d) Quenemer, D.; Chemtob, A.; Heroguez, V.; Gnanou, Y. *Polymer* **2005**, *46*, 1067–1075. (e) Also cf.: Lynn, D. M.; Kanaoka, S.; Grubbs, R. H. *J. Am. Chem. Soc.* **1996**, *118*, 784–790.
- (11) Review: Mecking, S.; Held, A.; Bauers, F. M. *Angew. Chem., Int. Ed.* **2002**, *41*, 544–561.
- (12) (a) Zuideveld, M.; Wehrmann, P.; Mecking, S. *Angew. Chem., Int. Ed.* **2004**, *43*, 869–873. (b) Bastero, A.; Kolb, L.; Wehrmann, P.; Bauers, F. M.; Göttker, I.; Monteil, V.; Thomann, R.; Chowdhry, M. M.; Mecking, S. *Polym. Mater. Sci. Eng.* **2004**, *90*, 740–741.
- (13) Hristov, I. H.; DeKock, R. L.; Anderson, G. D. W.; Göttker-Schnetmann, I.; Mecking, S.; Ziegler, T. *Inorg. Chem.* **2005**, *44*, 7806–7818.
- (14) Monitoring polymerization in emulsion by drawing of samples was hampered by foaming and clogging of the valve.
- (15) For propylene, 2, $\omega$  incorporation is identical to 1,2-incorporation.
- (16) This applies to chain running after a 1,2- as well as 2,1-insertion, cf. Scheme 1. The observed inactivity of **1** towards propylene indicates that also insertion into  $\text{M}-\text{CH}_2\text{CH}(\text{Me})\text{P}$  is slower than with **2** or **3** (a  $\text{M}-\text{CH}_2\text{CH}_2$  species cannot be formed in the case of propylene).

MA061462L